CLAIM AMENDMENTS

Amend Claims 1-9, and enter new Claims 10-14, as indicated in the following Listing of the Claims:

- (currently amended) A dividing wall column divided in the having a middle region which is divided into a feed section and an offtake section by a dividing wall and having as the following segments a) to h):
 - a) an upper column region,
 - an enrichment section of the feed section which enrichment section has a crosssectional area A_b,
 - a stripping section of the feed section which stripping section has a cross-sectional area A_e,
 - d) an upper part of the offtake section which upper part has a cross-sectional area Ad,
 - e) a lower part of the offtake section which lower part has a cross-sectional area Ae,
 - f) an intermediate region of the feed section,
 - g) an intermediate region of the offtake section and
 - a lower column region,

wherein where

the dividing wall is located vertically between the segments b) and d) and between the segments c) and e),

the segments b), d), c) and e) have separation-active internals,

and-the cross-sectional area A_b of the segment b) [3] is at least 10% smaller than the cross-sectional area A_d of segment d), and

the cross-sectional area A_c of the segment c) is at least 10% greater than the cross-sectional area A_c of segment e).

(currently amended) A The dividing wall column as elaimed in of claim 1, wherein the cross-sectional area A_b of the segment b) is at least 40%, preferably at least 60%; smaller than the cross-sectional area A_d of segment d).

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- (currently amended) A The dividing wall column as claimed in of claim 1, wherein the cross-sectional area A_c of the segment c) is at least 40%, preferably at least 60%, greater than the cross-sectional area A_c of segment c).
- 4. (currently amended) A The dividing wall column as elaimed in of claim 1, wherein the dividing wall is arranged obliquely between the segments f) and g) and forms an angle of from 25 to 75°, preferably from 55 to 65°, to the horizontal.
- 5. (currently amended) A The dividing wall column as claimed in of claim 1, wherein the having an operating pressure P is in the range from 0.0005 to 10 bar, and the calculated having ratios of the cross-sectional areas A'b/A'd and A'c/A'e are given calculated by the following relationships

$$\frac{A'_b}{A'_d} = \left(\frac{m_{s,b}}{m_{s,d}}\right) \times \left(\frac{m_{i,b}}{m_{i,d}}\right)^C$$

$$\frac{A'_{C}}{A'_{e}} = \left(\frac{m_{s,c}}{m_{s,e}}\right) \times \left(\frac{m_{i,c}}{m_{i,e}}\right)^{C}$$

wherein A'b, A'd, A'c, A'e are the cross-sectional areas of the segments b, d, c, e provided for the calculation:

 $m_{s,b}$, $m_{s,c}$, $m_{s,c}$, $m_{s,c}$ are the volume flows of gas through the segments b, d, c, e, measured in m^3/h :

 $m_{i,b},\,m_{i,d},\,m_{i,e},\,m_{i,e}$ are the volume flows of liquid through the segments b, d, c, e, measured in m^3/h , and

the exponent C is obtained as an operating-pressure-dependent variable from the an empirically determined function shown in Fig. 3, and

the calculated ratios A_b/A_d and A_c/A_e deviate from the corresponding, actual ratios A_b/A_d and A_c/A_e by not more than 30%, preferably not more than 20%.

(currently amended) A <u>The</u> dividing wall column as elaimed in of claim 1, wherein the <u>having an</u>
operating pressure is of from 0.0005 to 0.02 bar, and having liquid distributors in which the

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<u>provide a</u> liquid predistribution occurs by the <u>based on a bank-up principle and a the downstream fine liquid fine distribution occurs by the based on a capillary principle are used.</u>

- (currently amended) A <u>The</u> dividing wall column as elaimed in of claim 1, wherein the <u>separation-active internals are an</u> ordered packing having a cross-channel structure is used as separation active internals.
- 8. (currently amended) A The dividing wall column as claimed in of claim ± 6, wherein the separation-active internals are an ordered packing having a cross-channel structure, is used as separation active internals and the packing has an the uppermost packing layer of packing below the liquid distributor which is aligned so that the individual layers of the ordered packing are aligned parallel to the dividing wall.
- 9. (currently amended) A process for isolating pure purifying ethylhexyl p-methoxycinnamate which comprises distilling a feed mixture comprising from 70 to 95% of ethylhexyl p-methoxycinnamate as an intermediate-boiling fraction in the by distillation using a dividing wall column as etaimed in any of etaims 1 to 8 of claim 1, wherein the feed mixture introduced comprises from 70 to 95%, preferably from 75 to 90%, of ethylhexyl p-methoxycinnamate as intermediate boiling desired product.
- 10. (new) The dividing wall column of claim 1, wherein the cross-sectional area A_b of the segment b) is at least 60% smaller than the cross-sectional area A_d of segment d).
- 11. (new) The dividing wall column of claim 1, wherein the cross-sectional area A_c of the segment c) is at least 60% greater than the cross-sectional area of segment e).
- 12. (new) The dividing wall column of claim 1, wherein the dividing wall is arranged obliquely between the segments f) and g) and forms an angle of from 55 to 65° to the horizontal.
- 13. (new) The dividing wall column of claim 5, wherein the calculated ratios A'_b/A'_d and A'_c/A'_e deviate from the corresponding, actual ratios A_b/A_d and A_c/A_e by not more than 20%.

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14. (new) The process of claim 9, wherein the feed mixture comprises from 75 to 90% of ethylhexyl p-methoxycinnamate.

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